

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Cancelled)

Claim 2 (Currently Amended): The ~~desulfurization~~-method according to ~~Claim 1~~
~~1~~Claim 12, wherein the desulfurization conditions satisfy the following formula (2):

$$1.19 \times P_{\text{ope}}^{0.35} < T_{\text{ope}} / T_{50} < 1.68 \times P_{\text{ope}}^{0.24} \dots (2).$$

Claims 3-4 (Cancelled)

Claim 5 (Currently Amended): The ~~desulfurization~~-method according to ~~Claim 1~~
~~1~~Claim 12, wherein the metallic desulfurizing agent is a nickel-copper-based desulfurizing agent.

Claim 6 (Currently Amended): The ~~desulfurization~~-method according to ~~Claim 1~~
~~1~~Claim 12, wherein the liquid hydrocarbon comprises at least one member selected from the group consisting of a gasoline fraction, a kerosene fraction, and a gas oil fraction.

Claim 7 (Currently Amended): A method for producing hydrogen, said method comprising reforming a liquid hydrocarbon which has been desulfurized through said ~~desulfurization~~-method as recited in ~~Claim 1~~Claim 12 to produce said hydrogen.

Claim 8 (Previously Presented): The method for producing hydrogen according to Claim 7, wherein the reforming is partial-oxidation reforming, autothermal reforming, or steam reforming.

Claim 9 (Previously Presented): The method for producing hydrogen according to Claim 8, wherein said partial-oxidation reforming, said autothermal reforming, or said steam reforming is performed in the presence of a reforming catalyst comprising ruthenium or nickel.

Claim 10 (Previously Presented): The method for producing hydrogen for a fuel cell according to Claim 9, wherein the reforming catalyst comprises manganese oxide, cerium oxide, or zirconium oxide.

Claim 11 (Cancelled)

Claim 12 (Previously Presented): A method for producing a desulfurized liquid hydrocarbon, comprising:

identifying distillation characteristics of a liquid hydrocarbon;

selecting desulfurization conditions based on the distillation characteristics of the liquid hydrocarbon; and

contacting the liquid hydrocarbon with a metallic desulfurizing agent under the desulfurization conditions to obtain the desulfurized liquid hydrocarbon;

wherein:

selecting the desulfurization conditions comprises selecting conditions satisfying the following formula (1):

$$1.06 \times P_{\text{ope}}^{0.44} < T_{\text{ope}}/T_{50} < 1.78 \times P_{\text{ope}}^{0.22} \quad (1)$$

wherein

T_{ope} represents operation temperature in °C;

P_{ope} represents operation pressure in MPa; and

T_{50} represents a temperature per 50 percent recovered as determined by the "test method for distillation at atmospheric pressure" provided in the standard JIS K2254 "Petroleum products – Determination of distillation characteristics" as revised in 1998.

Claim 13 (New): The method according to Claim 12, wherein:

hydrogen addition is not employed while removing sulfur content; and

the metallic desulfurizing agent comprises a porous inorganic oxide and a metallic element comprising at least nickel (Ni) supported on the porous inorganic oxide